



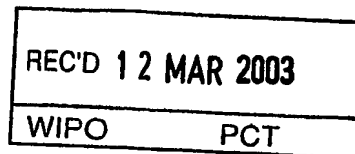
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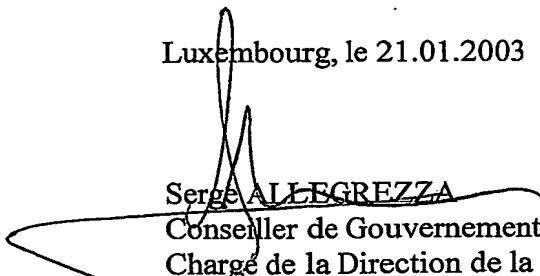
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Il est certifié par la présente que le document ci-annexé
(13 pages de description et 2 feuilles de dessin) est conforme à l'original de la demande de brevet
d'invention No. 90 883 déposée le 23.01.2002 auprès de la Direction de la Propriété Industrielle et
des Droits Intellectuels à Luxembourg, par PAUL WURTH S.A,

pour : Method and device for monitoring a mass flow in a pneumatic pipeline.

Luxembourg, le 21.01.2003


Serge ALLEGREZZA
Conseiller de Gouvernement 1ère classe
Chargé de la Direction de la Propriété Industrielle
et des Droits Intellectuels



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No.

Mémoire Descriptif
déposé à l'appui d'une demande de
BREVET D'INVENTION
au
Luxembourg

au nom de : **PAUL WURTH S.A.**
32, rue de l'Alsace
L-1122 Luxembourg / LU

pour : « Method and device for monitoring a mass flow in a pneumatic pipeline ».

METHOD AND DEVICE FOR MONITORING A MASS FLOW IN A PNEUMATIC PIPELINE

Field of the invention

The present invention relates to a method and device for monitoring a mass flow in a pneumatic pipeline.

Background of the invention

Pneumatic pipelines convey particulate solids, as e.g. pulverized or granular materials, using a gaseous fluid, usually air or an inert gas, as carrier medium. As pneumatic pipelines are becoming widespread in many areas of industry, there is an urgent need for simple and reliable methods and devices for monitoring a flow of particulate solids in a pneumatic pipeline and, more particularly, for monitoring the mass flow rate thereof. Being capable of continuously monitoring the mass flow rate in pneumatic pipelines allows for example: (i) to warrant an accurate delivery of particulate solids, thereby allowing to optimize a process and/or achieve a better product quality; (ii) to adjust optimum conveying conditions, thereby optimizing energy consumption and wear in the pneumatic conveying system; and (iii) to balance flow rates between multiple pipelines in complex pneumatic conveying systems.

Over the past three decades many different methods and devices have been developed for continuously monitoring the mass flow rate in a two phase solid/gas flow, including: mechanical, electrostatic, microwave, optical and acoustic methods. None of these methods is however a satisfactory solution for monitoring a flow of particulate solids in a pneumatic pipeline.

Mechanical methods use mechanical flow meters, such as: impact plates, multi-bladed rotors, Coriolis wheels, pressure drop measurement devices, as e.g. orifice plates and Venturi tubes. However, such mechanical flowmeters are generally unsuitable for monitoring the flow rate in pneumatic pipelines, be-

cause they are too sensitive to abrasion and present a risk of pipeline blockage.

Electrostatic flowmeters sense the electrostatic charge carried by the moving particles in pneumatic pipelines. A variety of factors, such as physical and chemical properties, humidity and velocity of the solid/gas flow, as well as configuration, material and wall roughness of the pipeline can influence their measures. Attempts have been made to improve accuracy by charging up the transported solid via an external electric source. However, this approach is considered unsuitable in many cases due to the risk of particulate explosion.

Microwave flowmeters generate electromagnetic waves in the GHz frequency range and measure how these electromagnetic waves are affected by the particulate solid flow in the pneumatic pipeline. A problem with the microwave flowmeters is that the electromagnetic field is generally not homogeneous over the whole cross section of the pipeline. The measurements may therefore be falsified by inhomogeneous flow regimes such as roping. Furthermore, microwave flowmeters are very sensitive to physical and chemical properties of the transported solids, and their measures are easily falsified by small depositions of solids.

Optical methods are based on light attenuation or scattering by the particulate solids flow. They are only applicable to gas/solids flows where solids concentration is very low and are therefore generally unsuitable for pneumatic pipelines.

Acoustic methods can be divided into active and passive acoustic methods. Active acoustic methods measure the attenuation of an incident ultrasonic beam by the solid particles conveyed in the pipeline. The main problem with the active acoustic methods is that they do not provide a homogeneous coverage of the whole cross section of the pipeline and that their measurements are therefore falsified by inhomogeneous flow regimes such as roping. Passive acoustic methods monitor the structure-borne acoustic waves generated by moving particles impacting upon or sliding along the pipe walls. The structure-borne acoustic waves are detected by microphones or piezoelectric sensors, which are strapped to the outer surface of the pipeline. Best results are ob-

tained if the acoustic sensors are mounted on the extrados surface of a bend in the pipeline. Usually a high frequency range is monitored to counteract the effects of mechanical noises conducted along the pipe. These passive acoustic methods are falsified by inhomogeneous flow regimes and by structure-borne
5 acoustic noise generated along the pneumatic pipeline.

Object of the invention

The technical problem underlying the present invention is to provide a simple, but reliable method and device for monitoring a particulate solids flow in a pneumatic pipeline.

Summary of the invention

The method in accordance with the present invention can be generally
10 qualified as a passive acoustic method. In contrast to known passive acoustic methods, the method does not sense structure-born acoustic waves directly produced by the particulate solids flow. In accordance with the invention, the particulate solids flow is first transformed into a free and compact solid/gas jet. This free and compact solid/gas jet is then intercepted by an impact body,
15 wherein it is warranted that the compact solid/gas jet impacts onto this impact body with substantially its whole cross-section. The compact solid/gas jet impacting onto the impact body generates structure-born acoustic waves in the impact body, which are sensed to monitor the mass flow of the particulate solids flow in the pneumatic pipeline. It will be appreciated that this method is
20 much less falsified by inhomogeneous flow regimes in the pneumatic pipeline and by structure-borne acoustic noise generated along the pneumatic pipeline than known passive acoustic methods.

The structure-born acoustic waves are normally sensed in one or more specific frequency ranges within the frequency range of 0 to 1000 kHz and
25 subjected to a frequency dependent analysis to derive therefrom a value that is representative of the mass flow rate of the particulate solids flow.

It will be appreciated that the impact body can be easily isolated from the

pneumatic pipeline with regard to structure-born acoustic noise. Thus, the structure-born acoustic waves that are sensed on the impact body cannot be falsified through structure-born acoustic noise in the pipeline.

The impact body is advantageously arranged within a measuring chamber
5 that is connected between an upstream section and a downstream section of the pneumatic pipeline. At the inlet of the measuring chamber, a nozzle transforms the particulate solids flow from the upstream section into a free, compact solid/gas jet, which impacts onto the impact body (34, 34') with substantially its whole cross-section. The particulate solids and the carrier gas
10 that are deflected by the impact body leave the measuring chamber to re-establish a particulate solids flow in the downstream section of the pneumatic pipeline.

To be protected against abrasion, the measuring chamber advantageously has a dead end that fills with particulate solids. In this embodiment, the
15 impact body has an impact head that is supported by a stem to protrude out of the particulate solids in the dead end.

A preferred device for monitoring the mass flow a particulate solids flow in a pneumatic pipeline comprises a measuring chamber, an impact body that is supported within the measuring chamber and an inlet connection. The latter is
20 designed to blow the particulate solids flow as a compact solid/gas jet onto the impact body, so that the compact solid/gas jet impacts onto the impact body with substantially its whole cross-section. An acoustic transducer is associated with the impact body for sensing structure-born acoustic waves, which are generated by said compact solid/gas jet impacting onto said impact body, and
25 converting them in an output signal.

Signal processing means are normally connected to the acoustic transducer for processing the output signal of the latter, so as to derive therefrom a measure of the mass flow rate of the particulate solids flow.

A preferred embodiment of the impact body includes a mounting plate for
30 mounting the impact body into the measuring chamber, a support stem centrally supported on the mounting plate and an impact head supported by the

support stem. This impact head forms an impact surface in axial prolongation of a central axis of the inlet connection. In a first embodiment, the impact head forms an impact surface that is substantially flat and perpendicular to the central axis of the inlet connection. In a preferred embodiment, the impact head
5 forms a convex, conical impact surface that is coaxial to the central axis of the inlet connection. The mounting plate closes the measuring chamber axially opposite the inlet connection, and the measuring chamber has an outlet opening laterally of the impact body. The inlet connection advantageous includes a nozzle for producing the compact solid/gas jet.

Brief description of the drawings

10 The present invention will now be described, by way of example, with reference to the accompanying drawings, in which:

Fig. 1: is a schematic section through a device in accordance with the present invention, for monitoring the mass flow of a particulate solids flow in a pneumatic pipeline; and

15 Fig. 2: is section through an alternative embodiment of an impact body for the device of Fig. 1.

Detailed description of a preferred embodiment

In Fig.1, reference number 10 identifies an upstream section and reference number 12 a downstream section of a pneumatic pipeline. Such a pneumatic pipeline is used to convey particulate materials, as e.g. pulverized or
20 granular materials, using a gaseous fluid, usually air or an inert gas, as carrier medium. Such a particulate solids flow is schematically identified by arrow 10', respectively 12'.

Reference number 14 globally identifies a device for monitoring the mass flow a particulate solids flow in the pneumatic pipeline 10', 12'. This device 14 is
25 connected between the upstream section 10 and the downstream section 12 of the pneumatic pipeline in replacement of a pipeline bend. It comprises a

measuring chamber 16 with an inlet connection 18 and an outlet connection 20. The central axes 18' and 20' of the inlet connection 18 and the outlet connection 20 are perpendicular to each other. The upstream section 10 of the pneumatic pipeline is axially connected to the inlet connection 18, and the downstream section 12 is axially connected to the outlet connection 20 of the measuring chamber 16. The inlet connection 18 axially opens into a conically diverging inlet chamber 22, which forms a transition into a cylindrical chamber 24 of the measuring chamber 16. This cylindrical chamber is coaxial to the central axis 18' of the inlet connection and has a much bigger free cross-section than the latter. The outlet connection 20 has an inlet opening 26 in a peripheral wall 28 of the cylindrical chamber 24.

Reference number 34 globally identifies an impact body, which includes a disk shaped mounting plate 36, a support stem 38 centrally supported on the mounting plate 36, and an impact head 40 supported by the support stem 38. The disk shaped mounting plate 36 is flanged with the help of an auxiliary flange 44 onto a flange 42 of the measuring chamber 16, so that it closes the latter axially opposite the inlet connection 18. Two damping rings 46, 48, which are made of a material having a good damping efficiency with regard to structure-born acoustic waves, isolate the mounting plate 36 (and consequently the impact body 34) from the measuring chamber 16 (and consequently from the pneumatic pipeline sections 10, 12), with regard to the transmission of structure-born acoustic noise.

The support stem 38 axially extends through the measuring chamber 16, to support the impact head 40 at the inlet of the cylindrical chamber 24 in axial prolongation of the central axis 18' of the inlet connection 18. In Fig. 1, the impact head 40 forms an impact surface 50, which is substantially flat and perpendicular to the central axis of the inlet connection 18.

A converging nozzle 52 is included in the inlet connection 18 to transform the particulate solids flow 10' in the upstream section 10 of the pneumatic pipeline in a compact solid/gas jet (not shown) that is axially blown into the measuring chamber 16 onto the impact surface 50. It will be noted that the

impact surface 50 is big enough to warrant that the compact solid/gas jet impacts onto this surface 50 with its whole cross-section.

The solid particles impacting onto the impact surface 50 generate structure-born acoustic waves in the impact body 34, which are measured by an acoustic transducer 52. The latter is in direct contact with an outer surface 54 of the mounting plate 36 of the impact body 34, in axial alignment with the support stem 38. As the impact body 34 is isolated from all other equipment with regard to structure-born acoustic noise, the acoustic transducer 52 only senses the structure-born acoustic waves which are generated by the compact solid/gas jet impacting with its whole cross-section onto the impact surface 50. These structure-born acoustic waves are then converted in an output signal 56 to be further processed and monitored. Depending on the characteristics of the particulate solids flow 10' to be monitored, the acoustic transducer 52 should allow a frequency analysis of the structure-born acoustic waves in the frequency range up to 1000 kHz. In some applications, it can be of interest to equip the impact body 34 with several acoustic transducers, each of these transducers being optimized for a particular frequency range.

Reference number 60 identifies a schematically represented signal processing equipment, to which the acoustic transducer 52 is connected. Such a signal processing equipment 60 comprises e.g. a computer, which processes the output signal 56 of the acoustic transducer 52 in real time. Special software filters and transforms the digitized output signal of the acoustic transducer 52 to derive therefrom a measure of the mass flow rate of the particulate solids flow. It will indeed be noted that the frequency and the amplitude of the structure-born acoustic waves sensed by the acoustic transducer 52 are representative of the number of impacts during a unit of time and of the mass of these particles, i.e. in other words of the mass flow rate of the particulate solids flow.

Referring again to the measuring chamber 16, it will be noted that the particles impacting onto the impact surface 50 will be deflected back into the measuring chamber 16. They will leave this measuring chamber 16 through the outlet connection 20, to form the particulate solids flow 12' in the downstream

section 12 of the pneumatic pipeline.

The measuring chamber 16 has a dead end 80 downstream of the inlet opening 26 of the outlet connection 20. This dead end 80 is filled up with the particulate material as schematically indicated by the dotted surface 82. It will
5 be appreciated that the material accumulated in this dead end 80 helps to protect the measuring chamber 16 against abrasion.

Fig. 2 represents an alternative embodiment of an impact body. This impact body 34' distinguishes from the impact body 34 of Fig. 1 mainly in that the impact head 40' forms a convex, conical impact surface 50' that is coaxial to the
10 central axis 18' of the inlet connection 18. This conical impact surface 50' radially deflects the solid particles impacting thereon. Such a radial deflection has the advantage that the deflected particles interfere to a lesser degree with the solid/gas jet before the latter impacts onto the impact surface 50'. In other
15 words, the compact solid/gas jet remains more compact and homogeneous than with the impact head 34 and less solid particles are prevented from impacting onto the impact surface 50'.

Claims

1. A method for monitoring the mass flow of a particulate solids flow in a pneumatic pipeline (10, 12), said method including a sensing of structure-born acoustic waves;
characterized by
 - 5 transforming said particulate solids flow into a free and compact solid/gas jet;
intercepting said compact solid/gas jet with an impact body (34, 34'), wherein said compact solid/gas jet impacts onto said impact body (34, 34') with substantially its whole cross-section; and
 - 10 sensing structure-born acoustic waves which are generated in said impact body (34,34') by said compact solid/gas jet impacting thereon, to monitor the mass flow of the particulate solids flow in the pneumatic pipeline.
2. The method as claimed in claim 1, wherein:
said structure-born acoustic waves are sensed in one or more specific frequency ranges within the frequency range of 0 to 1000 kHz and subjected to a frequency dependent analysis to derive therefrom a value that is representative of the mass flow rate of the particulate solids flow.
 - 15
3. The method as claimed in claim 1 or 2, wherein said impact body (34, 34') is isolated from the pneumatic pipeline with regard to structure-born acoustic noise.
 - 20
4. The method as claimed in anyone of claims 1 to 3, wherein:
said impact body (34, 34') is arranged within a measuring chamber (16) that is connected between an upstream section (10) and a downstream section (12) of said pneumatic pipeline;
 - 25 a nozzle (52) transforms said particulate solids flow from said upstream section (10) into a free, compact solid/gas jet, which impacts onto said impact body (34, 34') with substantially its whole cross-section; and

the particulate solids and the carrier gas that are deflected by said impact body (34, 34') leave said measuring chamber (16) to re-establish a particulate solids flow in said downstream section (12) of said pneumatic pipeline.

5. 5. The method as claimed in claim 4, wherein the particulate solids and the carrier gas that are deflected by said impact body (34, 34') leave said measuring chamber (16) through at least one lateral outlet opening (26) laterally of said impact body (34, 34').

6. The method as claimed in claim 5, wherein:

said impact body (34, 34') has an impact head (40);

10 said at least one lateral outlet opening (26) is arranged laterally of said impact head (40, 40') ;

said measuring chamber (16) has a dead end (80) that is filled up with particulate solids downstream of said lateral outlet opening (26); and

15 said impact head (40, 40') is supported by a stem so as to protrude out of said particulate solids in said dead end (80).

7. A device for monitoring the mass flow of a particulate solids flow in a pneumatic pipeline (10, 12), said device comprising an acoustic transducer (52) for sensing structure-born acoustic waves, **characterized by**

a measuring chamber (16);

20 an impact body (34, 34') that is supported within said measuring chamber (16);

an inlet connection (18) designed so as to blow said particulate solids flow as a compact solid/gas jet onto said impact body (34, 34'), so that said compact solid/gas jet impacts onto said impact body (34, 34') with substantially its whole cross-section ;

25 wherein said acoustic transducer (52) is associated with said impact body (34, 34') for sensing structure-born acoustic waves, which are generated by said compact solid/gas jet impacting onto said impact body (34, 34'), and converting them in an output signal.

8. The device as claimed in claim 7, further including:

signal processing means (60) for processing said output signal so as to derive therefrom a value that is representative of the mass flow rate of the particulate solids flow.

5 9. The device as claimed in claim 7 or 8, wherein said impact body (34, 34') is isolated from said measuring chamber (16) with regard to structure-born acoustic waves.

10. The device as claimed in anyone of claim 7 to 9, wherein said impact body (34, 34') includes:

10 a mounting plate (36, 36') for mounting said impact body (34, 34') in said measuring chamber (16);

a support stem (38, 38') centrally supported on said mounting plate (36); and

15 an impact head (40, 40') supported by said support stem (38, 38'), said impact head (40, 40') forming an impact surface (50, 50') in axial prolongation of a central axis of said inlet connection (18).

11. The device as claimed in claim 10, wherein said impact head (40, 40') forms an impact surface (50, 50') that is substantially flat and perpendicular to the central axis of said inlet connection (18).

20 12. The device as claimed in claim 10, wherein said impact head (40) forms a convex, conical impact surface (50, 50') that is coaxial to the central axis of said inlet connection (18).

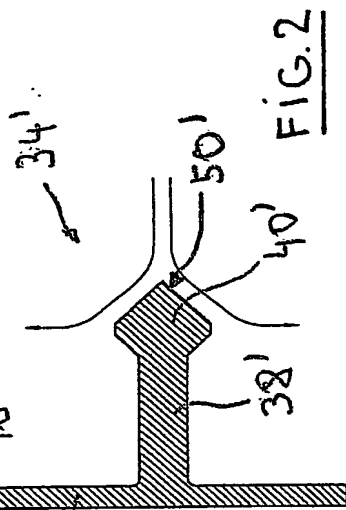
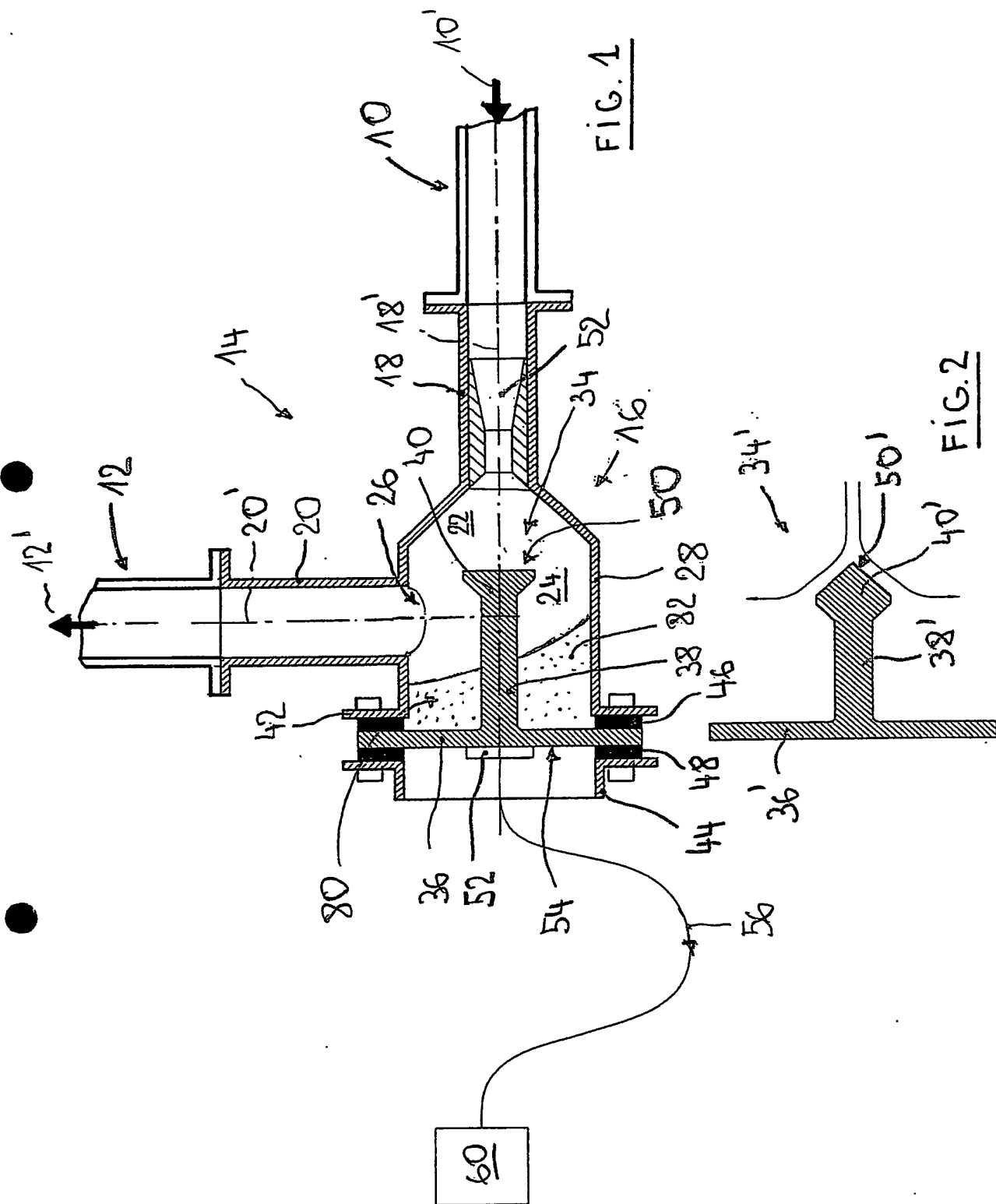
13. The device as claimed in anyone of claims 10 to 12, wherein :

25 said mounting plate (36) closes said measuring chamber (16) axially opposite said inlet connection (18); and

said measuring chamber (16) has a lateral outlet opening (26) laterally of said impact head (34, 34').
40, 40'

14. The device as claimed in claim 13, wherein said measuring chamber (16)

has a dead end (80) extending axially downstream of said lateral outlet opening (26).



Abstract

A device for monitoring the mass flow of a particulate solids flow in a pneumatic pipeline (10, 12) comprises a measuring chamber (16) and an impact body (34, 34'). Through an inlet connection (18) the particulate solids flow is blown as a compact solid/gas jet onto the impact body (34, 34'), so as to
5 impact thereon with substantially its whole cross-section. An acoustic transducer (52) is associated with the impact body (34, 34') for sensing structure-born acoustic waves, which are generated by said compact solid/gas jet impacting onto said impact body (34, 34'), and transforming them into an output
10 signal. Signal processing means (60) process the output signal so as to derive therefrom a value that is representative of the mass flow rate of the particulate solids flow.

(Figure 1)

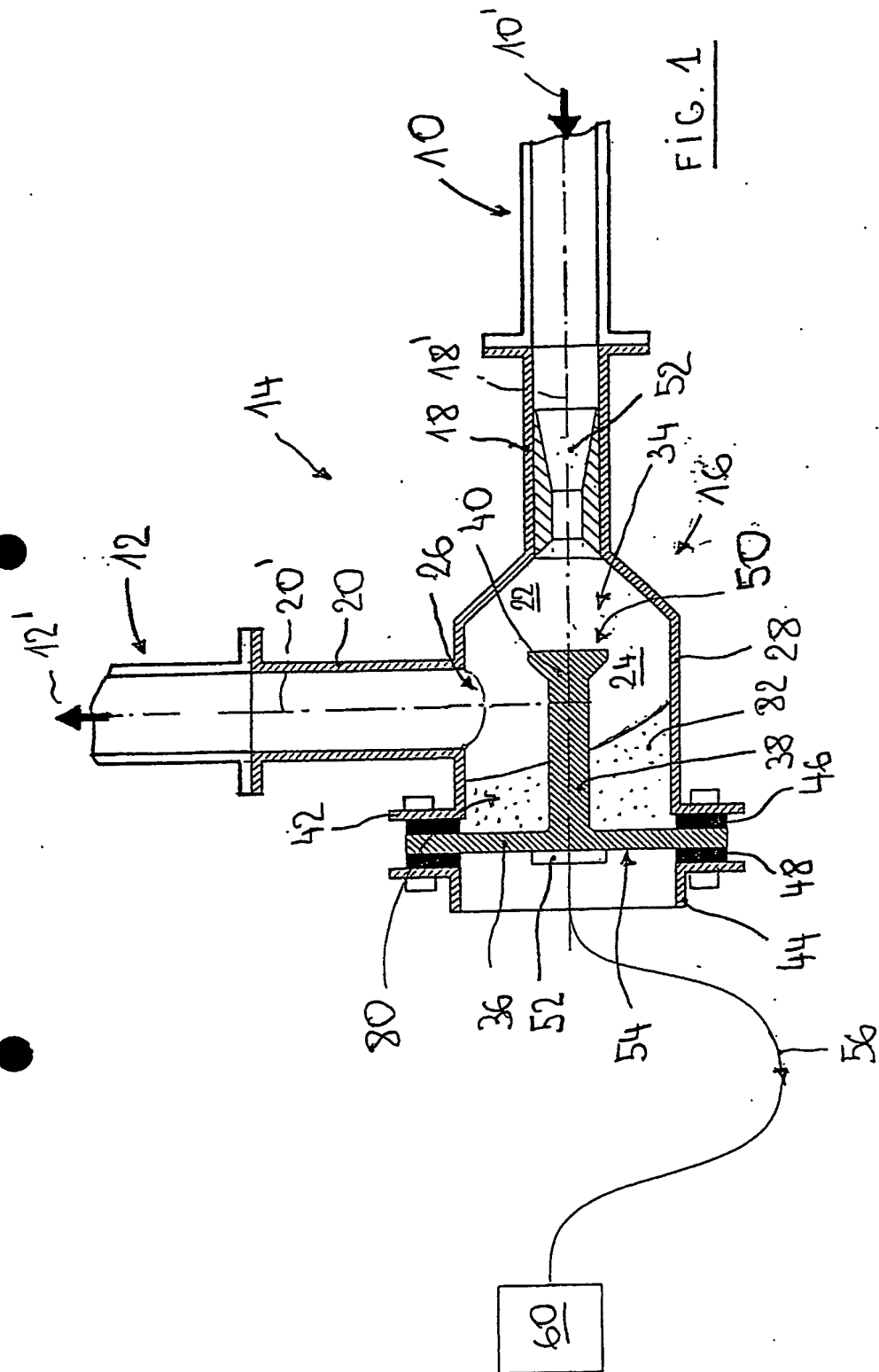


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